

Salt Partners

Economy of Ultrapure Salt Feedstock in Membrane Cell Chloralkali Plants

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Watch the video record of this presentation: www.youtube.com/watch?v=ELZ3SYrDqJE (25':44")

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Salt production world-wide

| Salt type | World production |
|------------------|-------------------------|
| Solar salt | 90'000'000 t/y |
| Rock salt | 80'000'000 t/y |
| Brines | 80'000'000 t/y |
| Total | 250'000'000 t/y |

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Salt consumption world-wide

| Salt user | Salt consumption |
|-------------------|------------------|
| Chemical industry | 150'000'000 t/y |
| Food | 60'000'000 t/y |
| Other | 40'000'000 t/y |

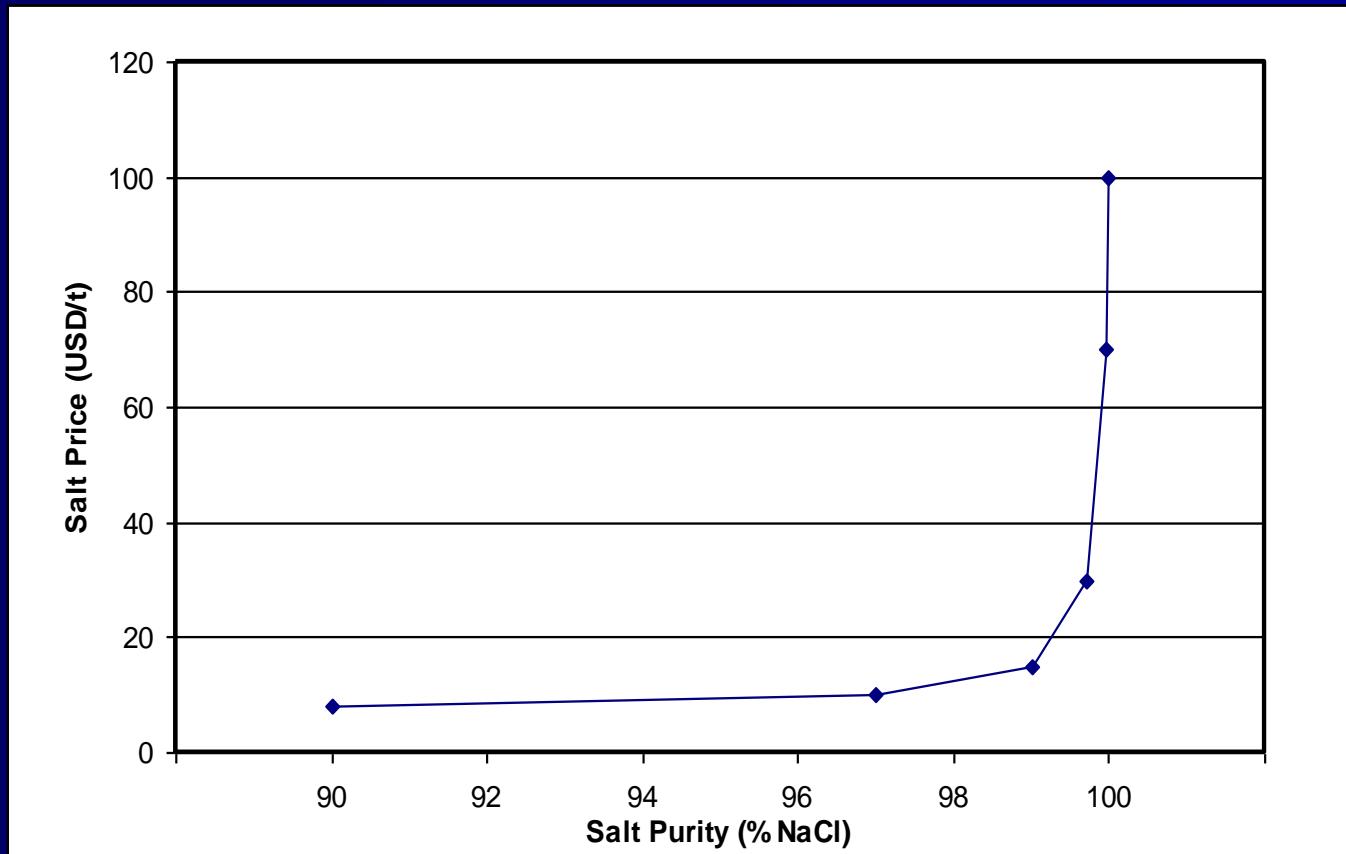
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Salt Purities

| | NaCl Purity (%) |
|----------------------------|-----------------------|
| Rock salt | 90 - 97 |
| Crude sea salt | 97 - 99 |
| Washed sea salt | 99 – 99.6 |
| Purified sea salt | 99.6 – 99.8 |
| Refined salt | 99.8 – 99.9 |
| Vacuum refined salt | 99.9 – 99.97 |
| Ultrapure salt | 99.97 – 99.997 |

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Salt Prices Depend on Salt Purity



Industrial
salt prices
vary between
USD 10.-/t
and
USD 100.-/t
depending
on salt purity

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Important Impurities in Salt in 1996

| | Rock salt | Sea salt | Lake salt | Brines |
|--------------------------|-----------|------------|-----------|-----------|
| CaSO_4 | 0.5 – 2% | 0.5 – 1% | 0.5 – 2% | Saturated |
| MgSO_4 | Traces | 0.2 – 0.6% | Traces | Traces |
| MgCl_2 | | 0.3 – 1% | Traces | |
| CaCl_2 | | | Traces | |
| Na_2SO_4 | | | Traces | |
| KCl | | | Traces | |
| NaBr | | | Traces | |
| Insolubles | 1 – 30% | 0.1 – 1% | 1 – 10% | |

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Important Impurities in Salt in 2012

Ag, Al, As, Ba, Br, Ca, Cd, Cr, Cu, F, Fe, Hg, I, K, Li, Mg, Mn, Mo, N (as NH₃ and as NO₂), Ni, P, Pb, S (as SO₄), Si (soluble), Si (total), Sr, Ti, V, Zn, TOC (Total Organic Carbon), Moisture, NORM (Naturally Occurring Radioactive Substances), Insolubles in 10% neutral brine, Insolubles in 2% neutral brine, Insolubles in alkaline brine, etc.

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Important Impurities in Brine for Membrane Cells

| | Max. | Membrane Licensor A | Membrane Licensor B |
|---------|------|---------------------|---------------------|
| Ca + Mg | ppb | 20 | 20 |
| SO4 | g/l | 5 | 4 - 8 |
| I | ppm | 0.1 | 0.2 |
| Ba | ppm | 0.1 | 0.5 |
| Sr | ppm | 0.4 | 0.1 |
| Al | ppm | 0.1 | 0.1 |
| SiO2 | ppm | 5 | 5 |
| Fe | ppm | 0.05 | 0.1 |
| Hg | ppm | 0.1 | 0.1 |
| Ni | ppm | 0.01 | 0.01 |
| Mn | ppm | - | 0.01 |
| F | ppm | - | 0.5 |
| TOC | ppm | 10 | 10 |

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The Basic Chloralkali Equation Caustic and Chlorine from Salt



| | | | | |
|------|----|----|----|---|
| 119 | 36 | 82 | 71 | 2 |
| 1.45 | | 1 | | |
| 1.68 | | | 1 | |

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The Basic Chloralkali Equation Soda Ash from Salt and Lime



| | | | |
|-----|-----|-----|-----|
| 119 | 110 | 111 | 120 |
|-----|-----|-----|-----|

| | | | |
|-----|------|---|--|
| 1.1 | 0.93 | 1 | |
|-----|------|---|--|

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Why must brine for chloralkali manufacture be pure?

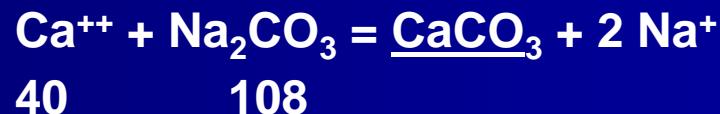
- Membrane damage in membrane cells
- Hydrogen evolution in Hg-cells
- Incrustations in soda ash production
- Contaminated effluents
- Bromine in chlorine for organic synthesis
- etc.

Brine for chloralkali manufacture must be purified.

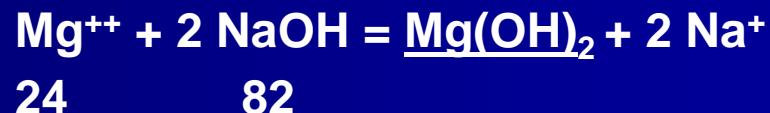
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Brine Purification: Ca and Mg Precipitation

Calcium precipitation



Magnesium precipitation



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Brine Purification: Overdosing of Reagents

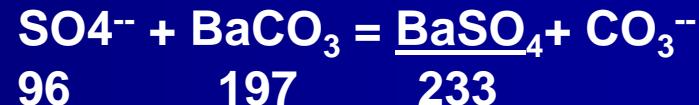
For calcium precipitation 0.4 kg Na₂CO₃ per m³ of brine

For magnesium precipitation 0.15 kg NaOH per m³ of brine

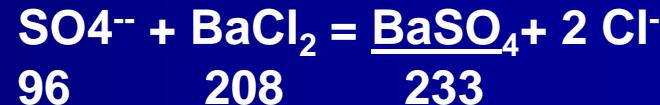
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Brine Purification: Sulphate Removal

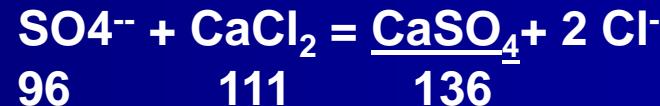
With BaCO_3



With BaCl_2



With CaCl_2

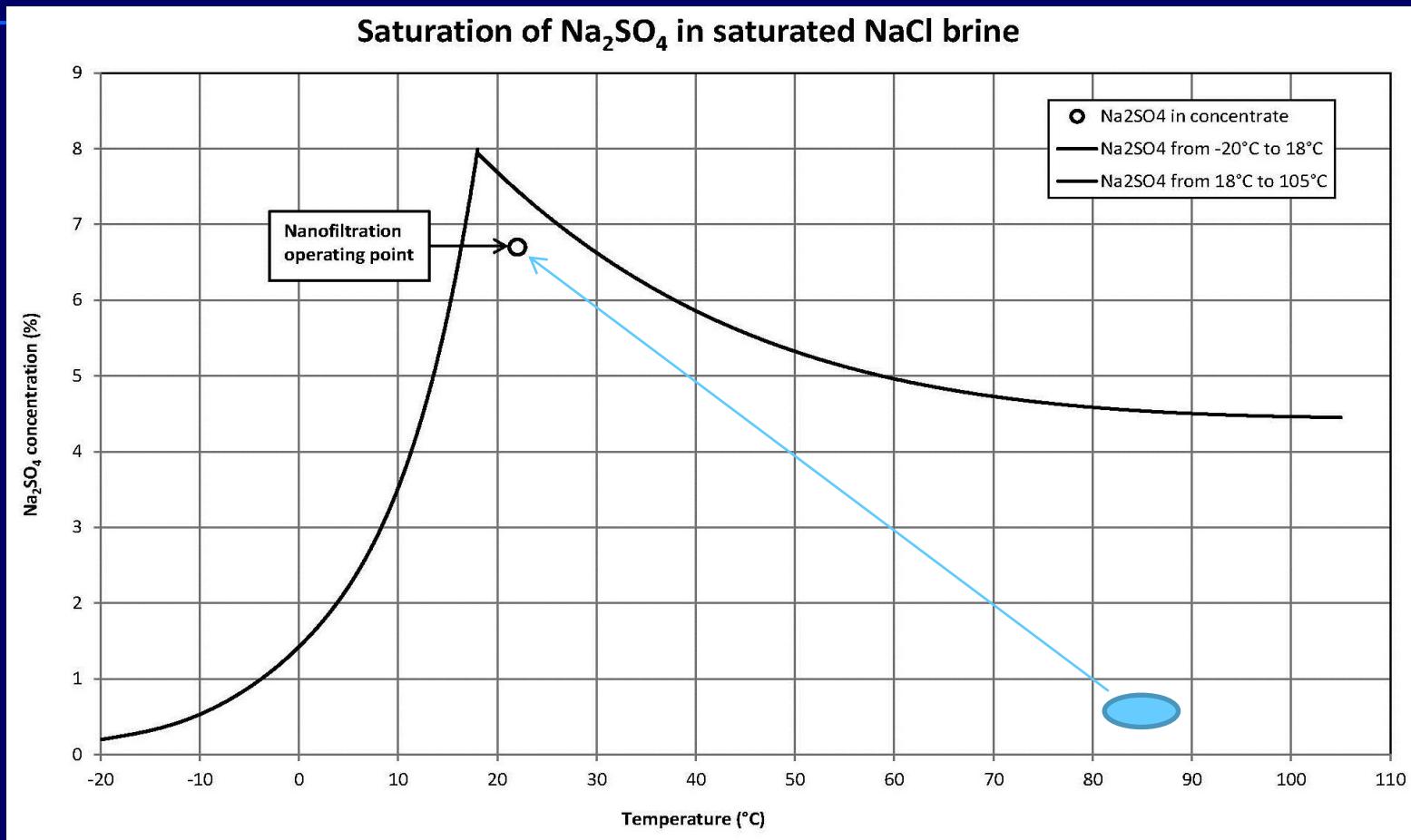


With Nanofiltration

From 4 – 8 g/l to 80 g/l in purge
as Na_2SO_4

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Nanofiltration Operating Point



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| Hellenic, Greece | Borsodchem, Hungary | Sind Alkalies, Pakistan | Frutaron, Israel |
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Cost of Salt and Brine Treatment

| | Cost of brine treatment and disposal (USD / t salt) | Cost of salt, brine treatment and disposal (USD / t salt) |
|----------------|--|--|
| Minimum | 1.50 | 10 |
| Average | 10 | 25 |
| Maximum | 30 | 50 |

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Relative Brine Treatment Cost

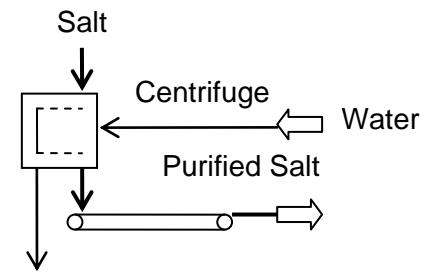
| | Cost of brine treatment as percentage of salt cost | Percentage of chloralkali production cost |
|----------------|--|---|
| | (%) | (%) |
| Minimum | 100 | 3 |
| Average | 170 | 15 |
| Maximum | 300 | 40 |

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HYDROSAL Process

**Centrifuge separates
salt and brine**

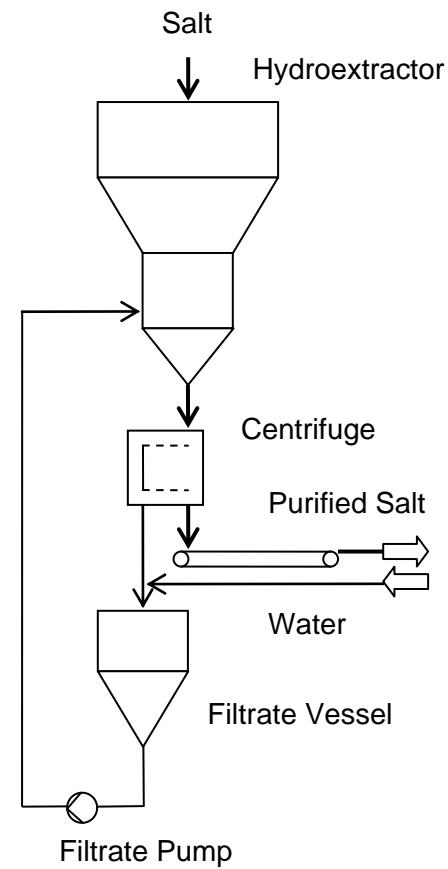
**Conventional
washing with water in
the centrifuge**



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HYDROSAL Process

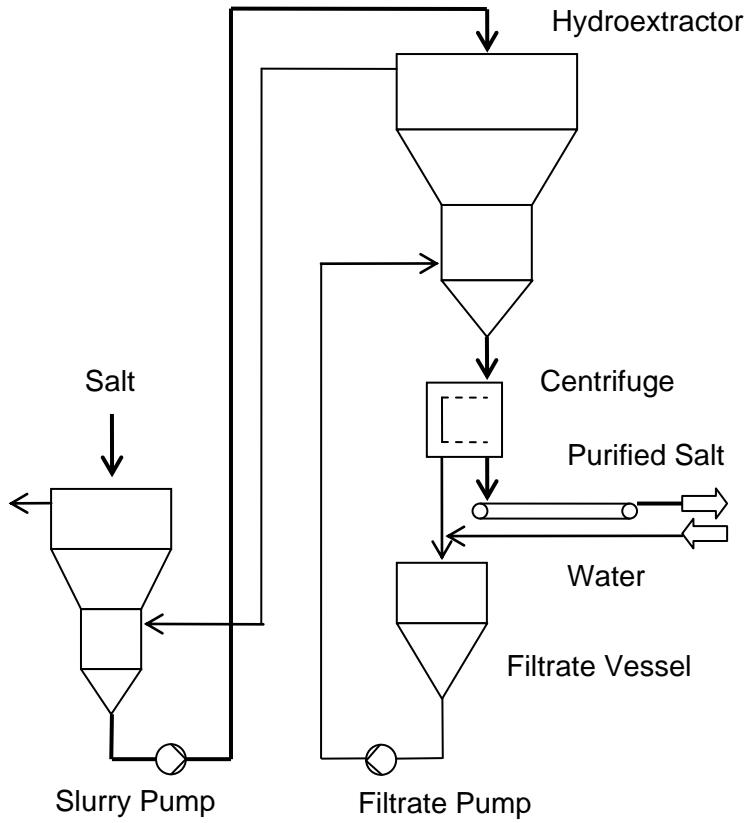
Dissolve salt fines in water and use this pure brine to remove impurities from salt in the hydroextractor



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HYDROSAL Process

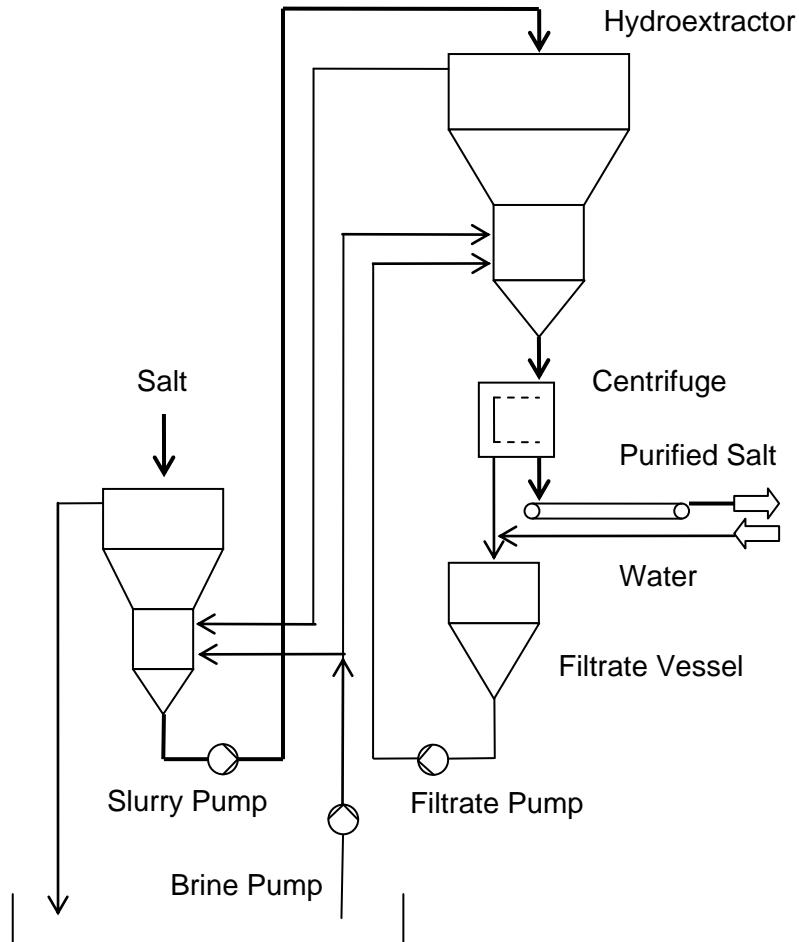
**Hydraulically
transport salt to the
hydroextractor and
return the transport
brine to the elutriator**



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HYDROSAL Process

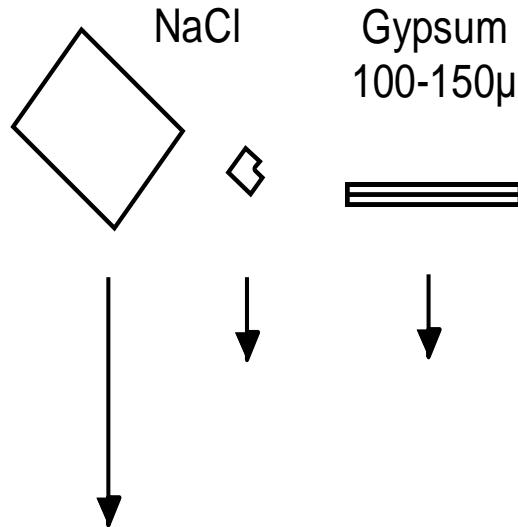
**Circulate impure
brine to control
hydroclassification
and elutriation
efficiency**



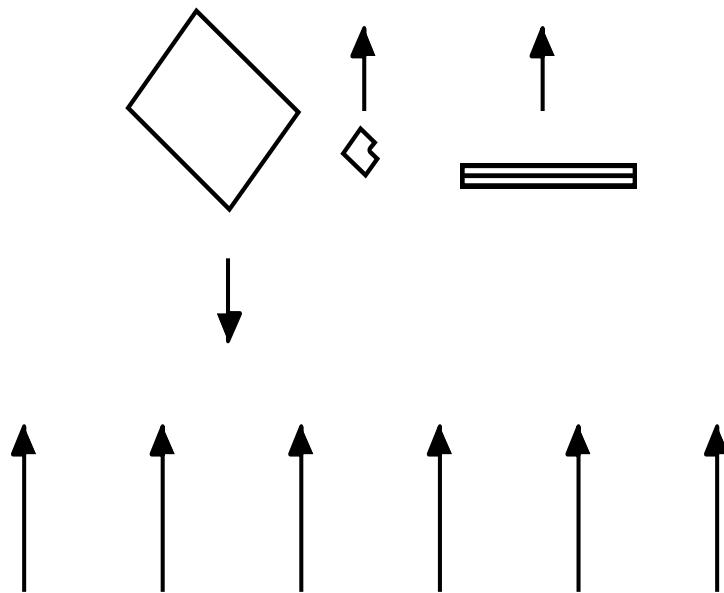
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Elutriation

Settling velocities in brine



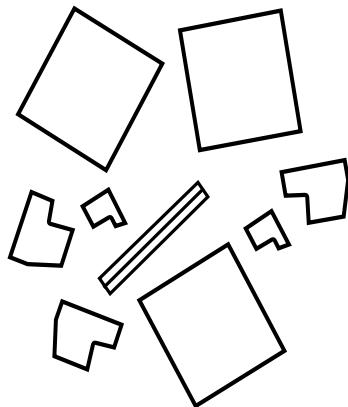
Elutriation in upwards flowing brine



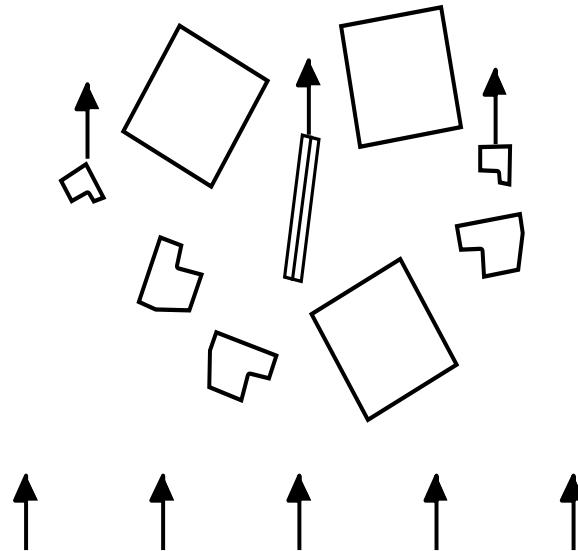
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Hydroclassification

Salt bed with buried impurities

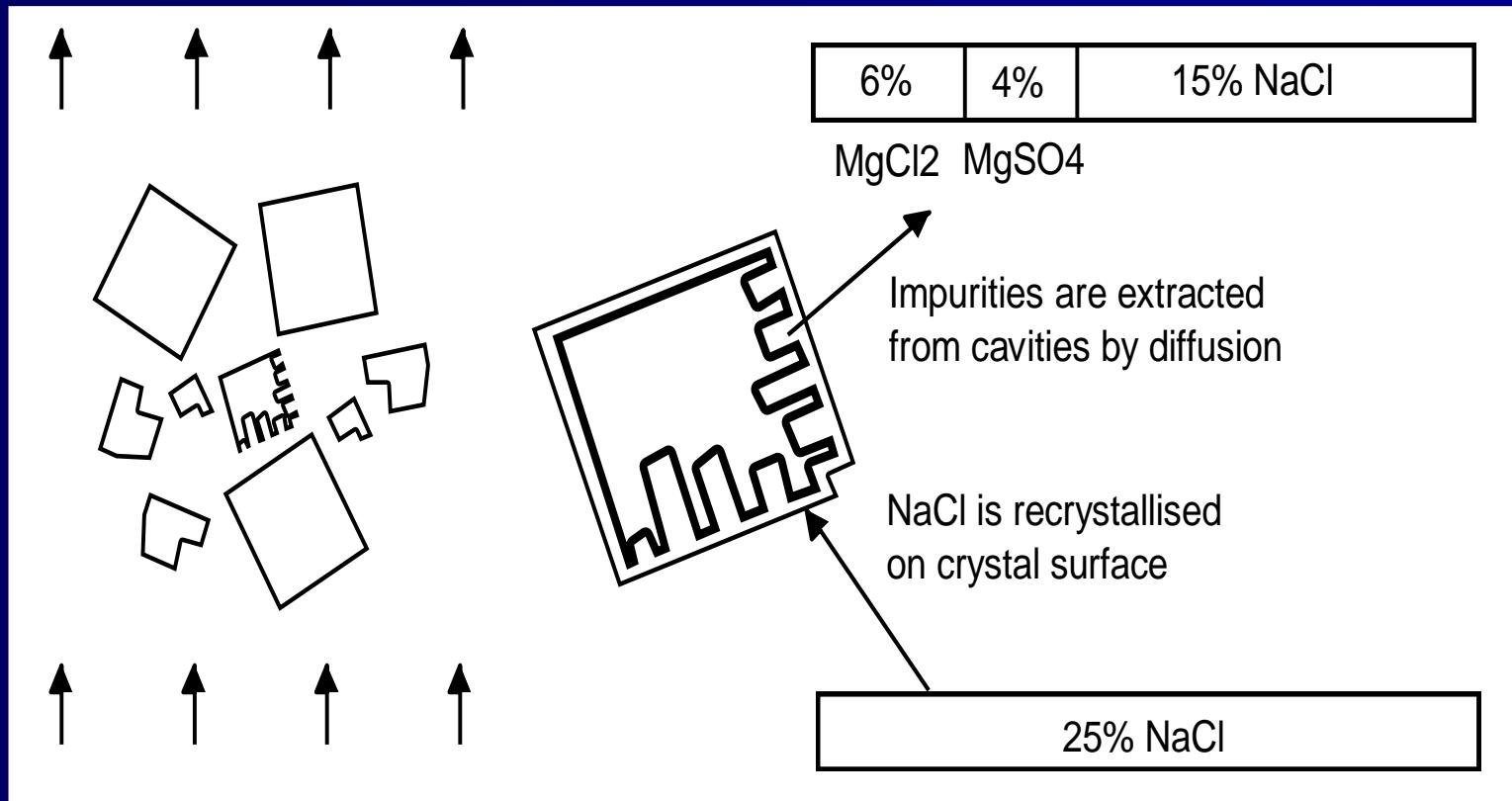


Hydroclassification of impurities
in partially fluidised salt bed



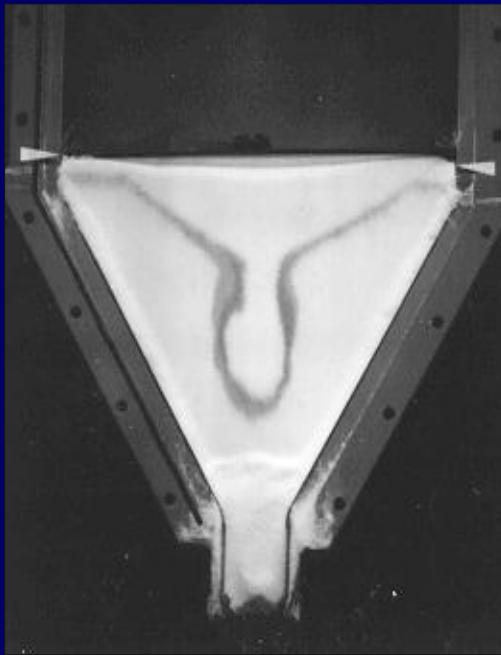
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Hydroextraction

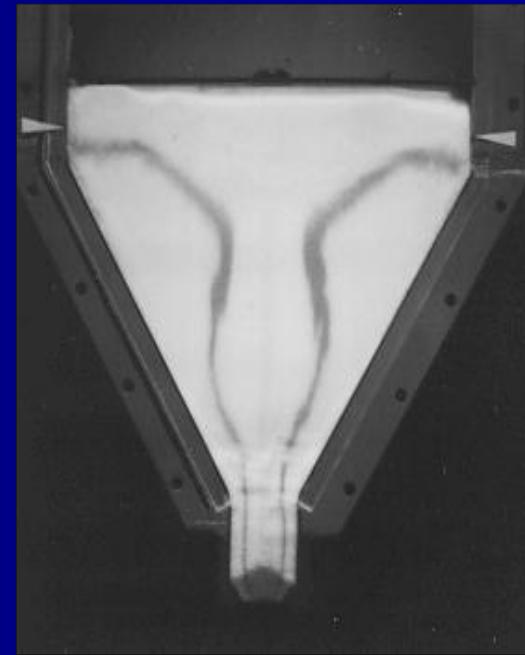


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Hydroextraction does not work in all vessels



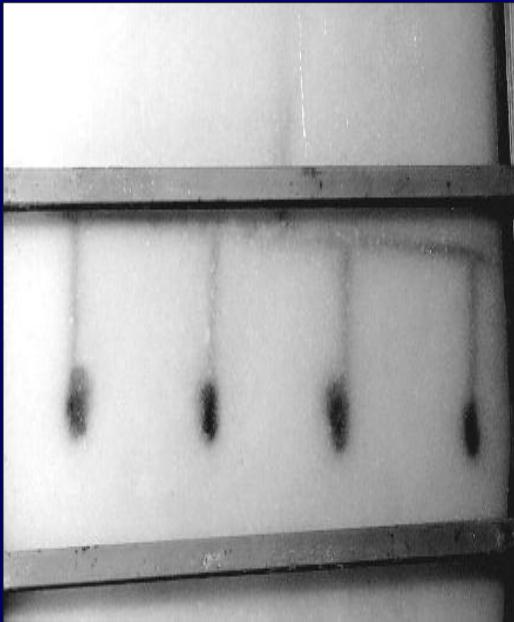
In this vessel salt flows out mainly through the centre



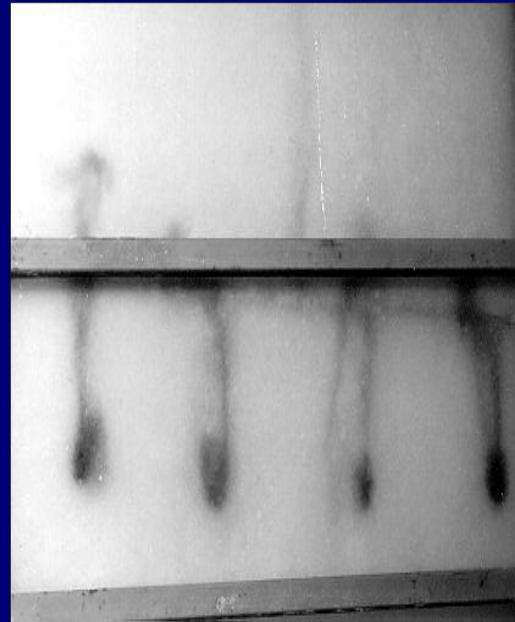
So called rat hole develops in the centre of the vessel

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Hydroextraction works only with plug flow of salt



Picture 1: Injection of black ink into brine flowing upwards through salt flowing downwards in plug flow



Picture 2: Black ink flows upwards with brine in counter-current flow



Picture 3: Second black ink injection. There are no traces of black colour in the salt flowing downwards in plug flow

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Solution mining for natural gas storage, co-generation, brine purification, salt crystallisation and refining plant in Portugal

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**40 t/h salt purification
plant in Portugal
producing purest
industrial salt in Europe**

| Performance test | | |
|------------------|-----|-----|
| Ca | ppm | 0.6 |
| Mg | ppm | 0.2 |
| SO4 | ppm | 53 |

Second International Flemion Seminar, Zurich,
Switzerland, 13. - 14. June 2012



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High quality European vacuum salt “A”
before and after HYDROSAL purification

| | | Commercial vacuum salt product | HYDROSAL purified |
|------------------|-----|-----------------------------------|-------------------|
| Ca | ppm | < 1 | < 1 |
| Mg | ppm | 0.12 | 0.07 |
| SO ₄ | ppm | 118 | 29 |
| K | ppm | 87 | 72 |
| Br | ppm | 35 | 34 |
| I | ppm | < 0.1 | < 0.1 |
| Ba | ppm | < 0.02 | < 0.02 |
| Sr | ppm | < 0.1 | < 0.1 |
| Al | ppm | < 0.05 | < 0.05 |
| SiO ₂ | ppm | 0.58 | 0.23 |

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High quality European vacuum salt “E”
before and after HYDROSAL purification

| | | Commercial vacuum salt product | HYDROSAL purified |
|------------------|-----|-----------------------------------|-------------------|
| Ca | ppm | 6.5 | 5.8 |
| Mg | ppm | 3.1 | 2.9 |
| SO ₄ | ppm | 191 | 33 |
| K | ppm | 36 | 29 |
| Br | ppm | 29 | 28 |
| I | ppm | < 0.1 | < 0.1 |
| Ba | ppm | < 0.02 | < 0.02 |
| Sr | ppm | 0.1 | < 0.1 |
| Al | ppm | < 0.05 | 0.05 |
| SiO ₂ | ppm | 0.81 | 0.47 |

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High quality European vacuum salt “N”
before and after HYDROSAL purification

| | | Commercial vacuum salt product | HYDROSAL purified |
|------------------|-----|-----------------------------------|-------------------|
| Ca | ppm | 211 | 66 |
| Mg | ppm | 6.8 | 1.2 |
| SO ₄ | ppm | 820 | 229 |
| K | ppm | 225 | 185 |
| Br | ppm | 43 | 36 |
| I | ppm | 0.4 | < 0.1 |
| Ba | ppm | 0.04 | < 0.02 |
| Sr | ppm | 6.3 | 2.2 |
| Al | ppm | 1.0 | 0.1 |
| SiO ₂ | ppm | < 0.1 | < 0.1 |

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Costs Related to Salt Use in Membrane Chloralkali Manufacture

- Salt Storage and Handling
- Salt Dissolution and Brine Purification
- Contaminated Sludge Handling and Disposal
- Purge Decontamination, Disposal and Salt Loss
- Ferrocyanide, Silica, Bromine and Iodine Removal
- Power Consumption
- Hydrochloric Acid Consumption
- Membrane Life
- Production Loss or Extra Production Capacity

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Comparative Study on Differential Costs in a Membrane Cell Plant having Following Parameters:

- Plant Capacity: 300'000 t/y of Chlorine
- Conversion from Mercury to Membranes
- Sulphate Removal with Nanofiltration
- Washed Salt with Bromine, Iodine and Ferrocyanide
- Ultrapure Salt without Bromine, Iodine and Ferrocyanide
- Ultrapure Salt in Silos, no Contamination
- Primary Brine Purification Plant Redundant
- Membrane Cells with Acidification
- Production Loss or Extra Production Capacity

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Membrane Plant Operation with Salt A and B

| | | Washed Salt A | Ultrapure Salt B |
|------------------|-----|---------------|------------------|
| Ca | (%) | 0.1 | 0.00005 |
| Mg | (%) | 0.01 | 0.00001 |
| SO4 | (%) | 0.4 | 0.003 |
| Insolubles | (%) | 0.5 | 0 |
| Moisture | (%) | 7 | 0.02 |
| NaCl (dry basis) | (%) | 98.9 | 99.996 |

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Membrane Plant Operation with Salt A and B

| | | Washed Salt A | Ultrapure Salt B |
|--|---------|-------------------|-------------------|
| Salt cost | (EUR/y) | 14'820'000 | 23'010'000 |
| Salt handling labour | (EUR/y) | 330'000 | 300'000 |
| Fuel | (EUR/y) | 40'000 | 0 |
| Salt handling maintenance | (EUR/y) | 80'000 | 120'000 |
| Process water | (EUR/y) | 20'000 | 330'000 |
| Brine purification chemicals | (EUR/y) | 1'170'000 | 50'000 |
| Primary brine purification power | (EUR/y) | 330'000 | 0 |
| Primary brine purification labour | (EUR/y) | 330'000 | 0 |
| Primary brine purif. maintenance | (EUR/y) | 300'000 | 0 |
| Solids disposal | (EUR/y) | 770'000 | 0 |

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Membrane Plant Operation with Salt A and B

| | | Washed Salt A | Ultrapure Salt B |
|--|---------|---------------|------------------|
| Nanofiltration plant cost | (EUR/y) | 800'000 | 0 |
| Nanofiltration power | (EUR/y) | 120'000 | 0 |
| Nanofiltration refrigeration water | (EUR/y) | 20'000 | 0 |
| Nanofiltration treated water | (EUR/y) | 40'000 | 0 |
| Nanofiltration reactants | (EUR/y) | 50'000 | 0 |
| Nanofiltration membrane replacement | (EUR/y) | 40'000 | 0 |
| Nanofiltration plant maintenance | (EUR/y) | 60'000 | 0 |
| Bromine removal | (EUR/y) | 1'500'000 | 0 |
| Ferrocyanide removal | (EUR/y) | 0 | 0 |
| Iodine removal | (EUR/y) | 0 | 0 |

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Membrane Plant Operation with Salt A and B

| | | Washed Salt A | Ultrapure Salt B |
|--|---------|-------------------|-------------------|
| Power consumption differential | (EUR/y) | 0 | - 830'000 |
| Hydrochloric acid differential | (EUR/y) | 0 | - 980'000 |
| Membrane life differential | (EUR/y) | 0 | - 220'000 |
| Plant depreciation differential | (EUR/y) | 0 | - 720'000 |
| Total | (EUR/y) | 21'060'000 | 21'060'000 |
| Salt delivered cost | (EUR/t) | 27.25 | 46.58 |
| Salt price differential | (EUR/t) | - | + 20.33 |
| Salt price differential | (%) | - | +74.6% |

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Conclusions:

- **Ultrapure salt makes primary brine purification redundant**
- **With ultrapure salt ,anion removal systems are not required**
- **With ultrapure salt, membrane life of up to 8 years is possible**
- **With ultrapure salt, plant operating cost is reduced**
- **With ultrapure salt, plant extra capacity is not required**
- **With ultrapure salt, loss of production is avoided**
- **Ultrapure salt can be EUR 20.33 / t or 74.6% more expensive than washed salt for the same chlorine production economy calculated in the example**
- **Each case must be examined considering specific costs**

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Thanks to Salt Partners Cost Survey Contributors

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Why not turn your salt into gold?



Vladimir M. Sedivy
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